



**EXTENDED NATURAL GAS ANALYSIS (*DHA)
GLYCALC INFORMATION**

PROJECT NO. :	202508079	ANALYSIS NO. :	01
COMPANY NAME :	QB ENERGY OPERATING, LLC	ANALYSIS DATE:	AUGUST 22, 2025 15:31
ACCOUNT NO. :		SAMPLE DATE :	AUGUST 08, 2028 08:30
PRODUCER :		CYLINDER NO. :	QB-1002
LEASE NO. :		SAMPLED BY :	NICK CROY
NAME/DESCRIP :	YCF 27-32-1 SURFACE CASING		

FIELD DATA		SAMPLE TEMP. :	
SAMPLE PRES. :	1345	AMBIENT TEMP.:	
H2S BY STAIN TUBE:	— ppm mol		
COMMENTS :			

<u>Componet</u>	<u>Mole %</u>	<u>Wt %</u>
Helium	0.00	0.00
Hydrogen	0.06	0.01
Carbon Dioxide	0.12	0.30
Nitrogen	0.16	0.25
Methane	90.4717	81.3977
Ethane	6.4562	10.8873
Propane	1.6717	4.1341
Isobutane	0.3514	1.1454
n-Butane	0.2430	0.7921
Isopentane	0.0527	0.2132
n-Pentane	0.0240	0.0971
Cyclopentane	0.0001	0.0004
n-Hexane	0.0027	0.0131
Cyclohexane	0.0001	0.0004
Other Hexanes	0.0094	0.0454
Heptanes	0.0006	0.0035
Methylcyclohexane	0.0001	0.0006
2,2,4 Trimethylpentane	0.0000	0.0000
Benzene	0.0000	0.0000
Toluene	0.0001	0.0005
Ethylbenzene	0.0001	0.0006
Xylenes	0.0004	0.0024
C8+ Heavies	0.0036	0.0333
<u>Subtotal</u>	<u>99.62790</u>	<u>99.32690</u>
Oxygen/Argon	0.00	0.00
Glycols	0.0006	0.0021
Alcohols	0.3715	0.6710
<u>Total</u>	<u>100.00000</u>	<u>100.00000</u>

	<u>Total</u>	<u>C6+</u>	<u>C8+</u>	<u>C10+</u>
<u>Calculated Values BTU @ 14.65</u>	<u>Sample</u>	<u>Fraction</u>	<u>Fraction</u>	<u>Fraction</u>
LHV Net Dry Real:	989.7	5287.2	7867.5	8644.5 Btu/scf
Net Wet Real:	972.4	5194.8	7730.0	8493.4 Btu/scf
HHV Gross Dry Real:	1096.3	5704.7	8481.2	9351.2 Btu/scf
Gross Wet Real:	1077.1	5605.0	8332.9	9187.7 Btu/scf

<u>Other Calculated Values</u>				
Regualr Wobbe Index*	1398.5	2992.9	3638.9	3843.0 Btu/scf
Net Heating Value (60 °F ideal reaction):	21084.2	19179.9	18924.6	19077.0 Btu/lbm
Gross Heating Value (60°F ideal reaction):	23348.4	20692.6	20393.6	20626.7 Btu/lbm
Molar Mass (MW):	17.82996	104.02	158.253	172.532 g/mol
Relative Density (AIR=1):	0.6152	3.5914	5.4638	5.9571 SG
Density:	0.04698	0.27411	0.41702	0.45465 lbm/scf
Compressibility Factor:	0.9975	0.9911	0.9998	0.9999 Z
Liquid Volume real gas @:	<u>14.65</u>	17.7373	0.005	0 gal/1000 scf

* The Wobbe pressure base in the number considered is based upon the given Pb of the HHV above.
 #DIV/0 or 0 (zero) will appear in the Calculated Value Section when there is no C6+, C8+ or C10+ in the sample to calculate these factors.
 BDL - Below Detection Limit. The H2S LOS has a detection limit of 0.25 ppm. A _ (an underscore) indicates there was no tube pulled for H2S.

The data presented herein has been acquired by means of current analytical techniques and represents the judicious conclusion EMPACT Analytical Systems, Inc. Results of the analysis can be affected by the sampling conditions, therefore, are only warranted through proper lab protocol. EMPACT assumes no responsibility for interpretation or any consequences from application of the reported information and is the sole liability of the user. The reproduction in any media of this reported information may not be made, in portion or as a whole, without the written permission of EMPACT Analytical Systems, Inc.



EXTENDED NATURAL GAS ANALYSIS (*DHA)

DHA COMPONENT LIST

PRIMARY DB KEY: 05-103-11104 NAME/DESCRIP : YCF 27-32-1
 LEASE #: SURFACE CASING
 FIELD/AREA:
 PROJECT NO. : 202508079 ANALYSIS NO. : 01
 COMPANY NAME : QB ENERGY OPERATING, LLC ANALYSIS DATE: AUGUST 22, 2025 15:31
 OFFICE / BRANCH: PARACHUTE, CO SAMPLE DATE : AUGUST 08, 2028 08:30
 CUSTOMER REF: TO:
 PRODUCER : EFFECTIVE DATE:

FIELD DATA

SAMPLE CYCLE: SAMPLE TYPE:
 SAMPLE PRES. : 1345 psig PROBE :
 FLOW PRES. : psig CYLINDER NO. : QB-1002
 LAB PRES: psig SAMPLED BY : NICK CROY
 SAMPLE TEMP. : °f SAMPLING COMPANY: QB ENERGY
 AMBIENT TEMP.: °f H2S BY STAIN TUBE: - ppm mol
 H2O BY STAIN TUBE: - #/mmcf CO2 BY STAIN TUBE: - Mol %
 FIELD COMMENTS:
 LAB COMMENTS:

COMPONENT	PIANO #	MOLE %	MASS %	GPM @ 14.65	GPM @ 14.73
Hydrogen	---	0.06	0.01	---	---
Nitrogen	---	0.16	0.25	---	---
Carbon Dioxide	---	0.12	0.30	---	---
Methane	P1	90.4717	81.3977	---	---
Ethane	P2	6.4562	10.8873	1.721	1.730
Propane	P3	1.6717	4.1341	0.459	0.461
i-Butane	I4	0.3514	1.1454	0.115	0.116
Methanol	X1	0.3700	0.6649	0.047	0.047
n-Butane	P4	0.2430	0.7921	0.076	0.076
2,2-Dimethylpropane	I5	0.0026	0.0105	0.001	0.001
i-Pentane	I5	0.0501	0.2027	0.018	0.018
Acetone	X3	0.0002	0.0007	0.000	0.000
n-Pentane	P5	0.0240	0.0971	0.009	0.009
t-Butanol	X4	0.0007	0.0029	0.000	0.000
2,2-Dimethylbutane	I6	0.0013	0.0063	0.001	0.001
Cyclopentane	N5	0.0001	0.0004	0.000	0.000
2,3-Dimethylbutane	I6	0.0011	0.0053	0.000	0.000
2-Methylpentane	I6	0.0049	0.0237	0.002	0.002
3-Methylpentane	I6	0.0018	0.0087	0.001	0.001
n-Hexane	P6	0.0027	0.0131	0.001	0.001
2-Butanol	X4	0.0006	0.0025	0.000	0.000
2,2-Dimethylpentane	I7	0.0001	0.0006	0.000	0.000
Methylcyclopentane	N6	0.0002	0.0009	0.000	0.000
2,4-Dimethylpentane	I7	0.0001	0.0006	0.000	0.000
Cyclohexane	N6	0.0001	0.0004	0.000	0.000
2-Methylhexane	I7	0.0001	0.0006	0.000	0.000
3-Methylhexane	I7	0.0001	0.0006	0.000	0.000
Ethylene glycol	GL2	0.0006	0.0021	0.000	0.000

UnknownC6s	U6	0.0001	0.0005	0.000	0.000
n-Heptane	P7	0.0002	0.0011	0.000	0.000
Methylcyclohexane	N7	0.0001	0.0006	0.000	0.000
Toluene	A7	0.0001	0.0005	0.000	0.000
n-Octane	P8	0.0001	0.0006	0.000	0.000
Ethylbenzene	I8	0.0001	0.0006	0.000	0.000
1,3-Dimethylbenzene (m-Xylene)	A8	0.0002	0.0012	0.000	0.000
1,4-Dimethylbenzene (p-Xylene)	A8	0.0001	0.0006	0.000	0.000
1,2-Dimethylbenzene (o-Xylene)	A8	0.0001	0.0006	0.000	0.000
i-Butylcyclopentane	N9	0.0001	0.0007	0.000	0.000
n-Nonane	P9	0.0001	0.0007	0.000	0.000
n-Propylbenzene	A9	0.0002	0.0013	0.000	0.000
3,6-Dimethyloctane	I10	0.0001	0.0008	0.000	0.000
3-Methylnonane	I10	0.0004	0.0032	0.000	0.000
n-Decane	P10	0.0001	0.0008	0.000	0.000
n-Undecane	P11	0.0006	0.0053	0.000	0.000
1,4-Ethyl-i-propylbenzene	A11	0.0001	0.0008	0.000	0.000
1,2-Methyl-n-butylbenzene	A11	0.0001	0.0008	0.000	0.000
n-Dodecane	P12	0.0003	0.0029	0.000	0.000
UnknownC12s	U12	0.0001	0.0009	0.000	0.000
n-Tridecane	P13	0.0006	0.0062	0.000	0.000
n-Tetradecane	P14	0.0001	0.0011	0.000	0.000
n-Pentadecane	P15	0.0005	0.0059	0.000	0.000
UnknownC16s	U16	0.0001	0.0013	0.000	0.000
TOTAL		100.00000	100.00000	2.4506	2.4639

CALCULATED VALUES**

BTEX COMPONENTS	MOLE%	WT%	BTU @	14.65	14.73
BENZENE	0.0000	0.0000	LHV NET DRY REAL :	989.7 /scf	995.1 /scf
TOLUENE	0.0001	0.0005	NET WET REAL :	972.4 /scf	977.8 /scf
ETHYLBENZENE	0.0001	0.0006	HHV GROSS DRY REAL :	1096.3 /scf	1102.2 /scf
XYLENES	0.0004	0.0024	GROSS WET REAL :	1077.1 /scf	1083.0 /scf
TOTAL BTEX	0.0006	0.0035	NET HEATING VALUE (60 °F ideal reaction):		21084.2 Btu/lbm
			GROSS HEATING VALUE (60°F ideal reaction):		23348.4 Btu/lbm
			RELATIVE DENSITY (AIR=1):		0.6152
			DENSITY		0.04698 lb/scf
			COMPRESSIBILITY FACTOR :		0.9975
			REGULAR WOBBE INDEX		1398.5

*(DETAILED HYDROCARBON ANALYSIS/NJ 1993)

Mod ASTM D6730, GPA 2261 & GPA 2286.

** (CALC: GPA 2172, GPA 2145 & TP-17 @14.696 & 60 F)

C6+ Fraction of DHA Gas Analysis @60°F, 14.696 psia

Net Dry Ideal BTU	<u>5256.8 /scf</u>	Relative Density - SG (Air=1)	<u>3.5914</u>	C6+ factors
Gross Dry Ideal BTU	<u>5671.9 /scf</u>	Z Compressibility Factor	<u>0.99114</u>	<u>0.98898</u>
Net Dry Ideal BTU	<u>19179.9 /lb</u>	Density Factor	<u>274.113 lbm/1000 ft3</u>	
Gross Dry Ideal BTU	<u>20692.6 /lb</u>	Molar Mass or MW	<u>104.02 g/mol</u>	
		Volume Liquid Ideal gas	<u>0.005 scf/gal</u>	<u>22.4</u>

This hexanes plus fraction may be applied in place of published C6+ factors. The Z & GPM need additional calc for C6+ factors. #DIV/0 or 0 (zero) will appear in this section when there is no hexanes plus in the sample to calculate C6+ factors.

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