



**EXTENDED NATURAL GAS ANALYSIS (*DHA)
GLYCALC INFORMATION**

PROJECT NO. :	202506058	ANALYSIS NO. :	04
COMPANY NAME :	QB ENERGY OPERATING, LLC	ANALYSIS DATE:	JUNE 19, 2025 20:19
ACCOUNT NO. :		SAMPLE DATE :	MAY 29, 2025
PRODUCER :	QB ENERGY OPERATING, LLC	CYLINDER NO. :	ECA-782
LEASE NO. :	COC-46029	SAMPLED BY :	MIKE KELLEY
NAME/DESCRIP :	RULISON FEDERAL 01-42 CASING		

FIELD DATA

SAMPLE PRES. :	336	SAMPLE TEMP. :	57
H2S BY STAIN TUBE:	—	AMBIENT TEMP.:	
COMMENTS :	—		

ppm mol
SPOT NO

Componet	Mole %	Wt %
Helium	0.01	0.00
Hydrogen	0.06	0.01
Carbon Dioxide	0.14	0.34
Nitrogen	0.10	0.15
Methane	90.3236	79.3880
Ethane	5.9813	9.8536
Propane	1.8521	4.4744
Isobutane	0.4001	1.2741
n-Butane	0.4161	1.3250
Isopentane	0.1823	0.7206
n-Pentane	0.1404	0.5550
Cyclopentane	0.0081	0.0311
n-Hexane	0.0739	0.3489
Cyclohexane	0.0425	0.1960
Other Hexanes	0.1408	0.6605
Heptanes	0.0675	0.3686
Methylcyclohexane	0.0319	0.1716
2,2,4 Trimethylpentane	0.0001	0.0006
Benzene	0.0183	0.0783
Toluene	0.0083	0.0419
Ethylbenzene	0.0000	0.0000
Xylenes	0.0000	0.0000
C8+ Heavies	0.0015	0.0094
Subtotal	99.99880	99.99760
Oxygen/Argon	0.00	0.00
Alcohols	0.0012	0.0024
Total	100.00000	100.00000

Calculated Values BTU @		Total Sample	C6+ Fraction	C8+ Fraction	C10+ Fraction	
	14.65					
LHV	Net Dry Real:	1014.7	4505.8	5564.0	#DIV/0!	Btu/scf
	Net Wet Real:	997.0	4427.0	5466.7	#DIV/0!	Btu/scf
HHV	Gross Dry Real:	1122.6	4845.0	5998.5	#DIV/0!	Btu/scf
	Gross Wet Real:	1103.0	4760.3	5893.6	#DIV/0!	Btu/scf

Other Calculated Values						
Regualr Wobbe Index*	1415.3	2746.7	3013.7	#DIV/0!		Btu/scf
Net Heating Value (60 °F ideal reaction):	21111.6	19205.8	19547.3	#DIV/0!		Btu/lbm
Gross Heating Value (60 °F ideal reaction):	23358.5	20653.9	21074.8	#DIV/0!		Btu/lbm
Molar Mass (MW):	18.25236	88.987	114.475	#DIV/0!		g/mol
Relative Density (AIR=1):	0.6298	3.0725	3.9524	#DIV/0!		SG
Density:	0.04809	0.23450	0.30166	#DIV/0!		lbm/scf
Compressibility Factor:	0.9974	0.9906	0.9957	#DIV/0!		Z
Liquid Volume real gas @:	14.65	17.8938	0.1485	0		0 gal/1000 scf

* The Wobbe pressure base in the number considered is based upon the given Pb of the HHV above.
 #DIV/0 or 0 (zero) will appear in the Calculated Value Section when there is no C6+, C8+ or C10+ in the sample to calculate these factors.
 BDL - Below Detection Limit. The H2S LOS has a detection limit of 0.25 ppm. A _ (an underscore) indicates there was no tube pulled for H2S.

The data presented herein has been acquired by means of current analytical techniques and represents the judicious conclusion EMPACT Analytical Systems, Inc. Results of the analysis can be affected by the sampling conditions, therefore, are only warranted through proper lab protocol. EMPACT assumes no responsibility for interpretation or any consequences from application of the reported information and is the sole liability of the user. The reproduction in any media of this reported information may not be made, in portion or as a whole, without the written permission of EMPACT Analytical Systems, Inc.



EXTENDED NATURAL GAS ANALYSIS (*DHA)

DHA COMPONENT LIST

PRIMARY DB KEY: **05-045-07185** NAME/DESCRIP : **RULISON FEDERAL 01-42**
 LEASE #: **COC-46029** CASING
 FIELD/AREA:

PROJECT NO. : **202506058** ANALYSIS NO. : **04**
 COMPANY NAME : **QB ENERGY OPERATING, LLC** ANALYSIS DATE: **JUNE 19, 2025 20:19**
 OFFICE / BRANCH: **PARACHUTE, CO** SAMPLE DATE : **MAY 29, 2025**
 CUSTOMER REF: TO:
 PRODUCER : **QB ENERGY OPERATING, LLC** EFFECTIVE DATE:

*****FIELD DATA*****

SAMPLE CYCLE: SAMPLE TYPE: **SPOT**
 SAMPLE PRES. : **336** psig PROBE : **NO**
 FLOW PRES. : psig CYLINDER NO. : **ECA-782**
 LAB PRES: psig SAMPLED BY : **MIKE KELLEY**
 SAMPLE TEMP. : **57** °f SAMPLING COMPANY: **QB ENERGY**
 AMBIENT TEMP.: °f H2S BY STAIN TUBE: **-** ppm mol
 H2O BY STAIN TUBE: **-** #/mmcf CO2 BY STAIN TUBE: **-** Mol %
 FIELD COMMENTS:
 LAB COMMENTS:

COMPONENT	PIANO #	MOLE %	MASS %	GPM @ 14.65	GPM @ 14.73
Helium	---	0.01	0.00	---	---
Hydrogen	---	0.06	0.01	---	---
Nitrogen	---	0.10	0.15	---	---
Carbon Dioxide	---	0.14	0.34	---	---
Methane	P1	90.3236	79.3880	---	---
Ethane	P2	5.9813	9.8536	1.595	1.604
Propane	P3	1.8521	4.4744	0.509	0.512
i-Butane	I4	0.4001	1.2741	0.131	0.132
Methanol	X1	0.0010	0.0017	0.000	0.000
n-Butane	P4	0.4160	1.3247	0.131	0.132
2,2-Dimethylpropane	I5	0.0052	0.0205	0.002	0.002
i-Pentane	I5	0.1771	0.7001	0.065	0.065
i-Propanol	X3	0.0001	0.0003	0.000	0.000
UnknownC4s	U4	0.0001	0.0003	0.000	0.000
n-Pentane	P5	0.1403	0.5546	0.051	0.051
t-Butanol	X4	0.0001	0.0004	0.000	0.000
2,2-Dimethylbutane	I6	0.0064	0.0302	0.003	0.003
Cyclopentane	N5	0.0081	0.0311	0.002	0.002
2,3-Dimethylbutane	I6	0.0121	0.0571	0.005	0.005
2-Methylpentane	I6	0.0542	0.2559	0.022	0.022
3-Methylpentane	I6	0.0303	0.1430	0.012	0.012
UnknownC5s	U5	0.0001	0.0004	0.000	0.000
n-Hexane	P6	0.0739	0.3489	0.030	0.030
2,2-Dimethylpentane	I7	0.0008	0.0044	0.000	0.000
Methylcyclopentane	N6	0.0378	0.1743	0.013	0.013
2,4-Dimethylpentane	I7	0.0033	0.0181	0.002	0.002
2,2,3-Trimethylbutane	I7	0.0008	0.0044	0.000	0.000
Benzene	A6	0.0183	0.0783	0.005	0.005

3,3-Dimethylpentane	I7	0.0010	0.0055	0.000	0.000
Cyclohexane	N6	0.0425	0.1960	0.014	0.014
2-Methylhexane	I7	0.0092	0.0505	0.004	0.004
2,3-Dimethylpentane	I7	0.0068	0.0373	0.003	0.003
1,1-Dimethylcyclopentane	N7	0.0029	0.0156	0.001	0.001
3-Methylhexane	I7	0.0106	0.0582	0.005	0.005
1c,3-Dimethylcyclopentane	N7	0.0043	0.0231	0.002	0.002
1t,3-Dimethylcyclopentane	N7	0.0037	0.0199	0.002	0.002
3-Ethylpentane	I7	0.0009	0.0049	0.000	0.000
1t,2-Dimethylcyclopentane	N7	0.0054	0.0290	0.002	0.002
2,2,4-Trimethylpentane	I8	0.0001	0.0006	0.000	0.000
n-Heptane	P7	0.0166	0.0911	0.008	0.008
1c,2-Dimethylcyclopentane	N7	0.0002	0.0011	0.000	0.000
Methylcyclohexane	N7	0.0319	0.1716	0.013	0.013
2,2-Dimethylhexane	I8	0.0004	0.0025	0.000	0.000
1,1,3-Trimethylcyclopentane	N7	0.0002	0.0012	0.000	0.000
Ethylcyclopentane	N7	0.0008	0.0043	0.000	0.000
2,5-Dimethylhexane	I8	0.0002	0.0013	0.000	0.000
2,2,3-Trimethylpentane	I8	0.0002	0.0013	0.000	0.000
1c,2t,4-Trimethylcyclopentane	N8	0.0002	0.0012	0.000	0.000
Toluene	A7	0.0083	0.0419	0.003	0.003
2,3-Dimethylhexane	I8	0.0001	0.0006	0.000	0.000
2-Methylheptane	I8	0.0001	0.0006	0.000	0.000
1c,2t,3-Trimethylcyclopentane	N8	0.0001	0.0006	0.000	0.000
1t,4-Dimethylcyclohexane	N8	0.0001	0.0006	0.000	0.000
1,1,4-Trimethylcyclohexane	N9	0.0001	0.0007	0.000	0.000
TOTAL		100.0000	100.0000	2.6346	2.6487

CALCULATED VALUES**

BTEX COMPONENTS	MOLE%	WT%	BTU @	14.65	14.73
BENZENE	0.0183	0.0783	LHV NET DRY REAL :	1014.7 /scf	1020.2 /scf
TOLUENE	0.0083	0.0419	NET WET REAL :	997.0 /scf	1002.5 /scf
ETHYLBENZENE	0.0000	0.0000	HHV GROSS DRY REAL :	1122.6 /scf	1128.7 /scf
XYLENES	0.0000	0.0000	GROSS WET REAL :	1103.0 /scf	1109.1 /scf
TOTAL BTEX	0.0266	0.1202	NET HEATING VALUE (60 °F ideal reaction):		21111.6 Btu/lbm
			GROSS HEATING VALUE (60°F ideal reaction):		23358.5 Btu/lbm
			RELATIVE DENSITY (AIR=1):		0.6298
			DENSITY		0.04809 lb/scf
			COMPRESSIBILITY FACTOR :		0.9974
			REGULAR WOBBE INDEX		1415.3

*(DETAILED HYDROCARBON ANALYSIS/NJ 1993)

Mod ASTM D6730, GPA 2261 & GPA 2286.

** (CALC: GPA 2172, GPA 2145 & TP-17 @14.696 & 60 F)

C6+ Fraction of DHA Gas Analysis @60°F, 14.696 psia

Net Dry Ideal BTU	<u>4477.5 /scf</u>	Relative Density - SG (Air=1)	<u>3.0725</u>	C6+ factors
Gross Dry Ideal BTU	<u>4814.6 /scf</u>	Z Compressibility Factor	<u>0.99061</u>	<u>0.99013</u>
Net Dry Ideal BTU	<u>19205.8 /lb</u>	Density Factor	<u>234.497 lbm/1000 ft3</u>	
Gross Dry Ideal BTU	<u>20653.9 /lb</u>	Molar Mass or MW	<u>88.987 g/mol</u>	
		Volume Liquid Ideal gas	<u>0.149 scf/gal</u>	<u>25.5</u>

**This hexanes plus fraction may be applied in place of published C6+ factors. The Z & GPM need additional calc for C6+ factors.
#DIV/0 or 0 (zero) will appear in this section when there is no hexanes plus in the sample to calculate C6+ factors.**

The data presented herein has been acquired by means of current analytical techniques and represents the judicious conclusion EMPACT Analytical Systems, Inc. Results of the analysis can be affected by the sampling conditions, therefore, are only warranted through proper lab protocol. EMPACT assumes no responsibility for interpretation or any consequences from application of the reported information and is the sole liability of the user. The reproduction in any media of this reported information may not be made, in portion or as a whole, without the written permission of EMPACT Analytical Systems, Inc.