



**EXTENDED NATURAL GAS ANALYSIS (*DHA)
GLYCALC INFORMATION**

PROJECT NO. :	202502080	ANALYSIS NO. :	04
COMPANY NAME :	QB ENERGY OPERATING, LLC	ANALYSIS DATE:	FEBRUARY 27, 2025 16:46
ACCOUNT NO. :		SAMPLE DATE :	FEBRUARY 18, 2025
PRODUCER :	QB ENERGY OPERATING, LLC	CYLINDER NO. :	ECA-798
LEASE NO. :		SAMPLED BY :	MIKE KELLEY
NAME/DESCRIP :	110180057 596-29C 21 CASING		

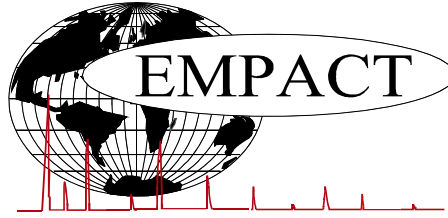
FIELD DATA		SAMPLE TEMP. :	33
SAMPLE PRES. :	331	AMBIENT TEMP.:	
H2S BY STAIN TUBE:	—		
COMMENTS :	<i>SPOT</i>		<i>NO PROBE</i>

<u>Componet</u>	<u>Mole %</u>	<u>Wt %</u>
Helium	0.00	0.00
Hydrogen	1.20	0.13
Carbon Dioxide	4.13	9.72
Nitrogen	0.06	0.09
Methane	87.1864	74.8034
Ethane	4.9985	8.0382
Propane	1.1596	2.7347
Isobutane	0.3061	0.9515
n-Butane	0.5168	1.6065
Isopentane	0.1405	0.5421
n-Pentane	0.0728	0.2809
Cyclopentane	0.0039	0.0147
n-Hexane	0.0327	0.1507
Cyclohexane	0.0139	0.0626
Other Hexanes	0.0867	0.3977
Heptanes	0.0403	0.2149
Methylcyclohexane	0.0181	0.0950
2,2,4 Trimethylpentane	0.0001	0.0006
Benzene	0.0129	0.0539
Toluene	0.0093	0.0458
Ethylbenzene	0.0001	0.0006
Xylenes	0.0008	0.0045
C8+ Heavies	0.0095	0.0582
<u>Subtotal</u>	<u>99.99900</u>	<u>99.99650</u>
Oxygen/Argon	0.00	0.00
Alcohols	0.0010	0.0035
<u>Total</u>	<u>100.00000</u>	<u>100.00000</u>

	<u>Total</u>	<u>C6+</u>	<u>C8+</u>	<u>C10+</u>	
Calculated Values BTU @	14.65				
LHV Net Dry Real:	945.9	4566.5	5667.6	#DIV/0!	Btu/scf
Net Wet Real:	929.4	4486.7	5568.5	#DIV/0!	Btu/scf
HHV Gross Dry Real:	1047.5	4908.6	6097.4	#DIV/0!	Btu/scf
Gross Wet Real:	1029.2	4822.8	5990.8	#DIV/0!	Btu/scf
Other Calculated Values					
Regualr Wobbe Index*	1304.9	2761.7	3081.4	#DIV/0!	Btu/scf
Net Heating Value (60 °F ideal reaction):	19218.9	19185.6	19762.4	#DIV/0!	Btu/lbm
Gross Heating Value (60°F ideal reaction):	21283.2	20622.7	21263.7	#DIV/0!	Btu/lbm
Molar Mass (MW):	18.69824	90.381	113.403	#DIV/0!	g/mol
Relative Density (AIR=1):	0.6453	3.1205	3.9158	#DIV/0!	SG
Density:	0.04927	0.23817	0.29883	#DIV/0!	lbm/scf
Compressibility Factor:	0.9975	0.9908	0.9969	#DIV/0!	Z
Liquid Volume real gas @:	14.65	17.5888	0.0887	0.003	0 gal/1000 scf

* The Wobbe pressure base in the number considered is based upon the given Pb of the HHV above.
 #DIV/0 or 0 (zero) will appear in the Calculated Value Section when there is no C6+, C8+ or C10+ in the sample to calculate these factors.
 BDL - Below Detection Limit. The H2S LOS has a detection limit of 0.25 ppm. A _ (an underscore) indicates there was no tube pulled for H2S.

The data presented herein has been acquired by means of current analytical techniques and represents the judicious conclusion EMPACT Analytical Systems, Inc. Results of the analysis can be affected by the sampling conditions, therefore, are only warranted through proper lab protocol. EMPACT assumes no responsibility for interpretation or any consequences from application of the reported information and is the sole liability of the user. The reproduction in any media of this reported information may not be made, in portion or as a whole, without the written permission of EMPACT Analytical Systems, Inc.



**EXTENDED NATURAL GAS ANALYSIS (*DHA)
DHA COMPONENT LIST**

PRIMARY DB KEY:	05-045-18087	NAME/DESCRIP :	110180057 596-29C 21
LEASE #:		CASING	
FIELD/AREA:			
PROJECT NO. :	202502080	ANALYSIS NO. :	04
COMPANY NAME :	QB ENERGY OPERATING, LLC	ANALYSIS DATE:	FEBRUARY 27, 2025 16:46
OFFICE / BRANCH:	PARACHUTE, CO	SAMPLE DATE :	FEBRUARY 18, 2025
CUSTOMER REF:		TO:	
PRODUCER :	QB ENERGY OPERATING, LLC	EFFECTIVE DATE:	

FIELD DATA

SAMPLE CYCLE:		SAMPLE TYPE:	SPOT
SAMPLE PRES. :	331	PROBE :	NO
FLOW PRES. :		CYLINDER NO. :	ECA-798
LAB PRES:		SAMPLED BY :	MIKE KELLEY
SAMPLE TEMP. :	33	SAMPLING COMPANY:	QB ENERGY
AMBIENT TEMP.:		H2S BY STAIN TUBE:	- ppm mol
H2O BY STAIN TUBE:	-	CO2 BY STAIN TUBE:	- Mol %

FIELD COMMENTS:
LAB COMMENTS:

COMPONENT	PIANO #	MOLE %	MASS %	GPM @	
				14.65	14.73
Hydrogen	---	1.20	0.13	---	---
Nitrogen	---	0.06	0.09	---	---
Carbon Dioxide	---	4.13	9.72	---	---
Methane	P1	87.1864	74.8034	---	---
Ethane	P2	4.9985	8.0382	1.332	1.339
Propane	P3	1.1596	2.7347	0.319	0.321
i-Butane	I4	0.3061	0.9515	0.100	0.101
n-Butane	P4	0.2244	0.6976	0.071	0.071
2,2-Dimethylpropane	I5	0.0047	0.0181	0.002	0.002
i-Pentane	I5	0.1358	0.5240	0.050	0.050
i-Propanol	X3	0.0006	0.0019	0.000	0.000
UnknownC4s	U4	0.2924	0.9089	0.092	0.092
n-Pentane	P5	0.0728	0.2809	0.026	0.026
t-Butanol	X4	0.0004	0.0016	0.000	0.000
2,2-Dimethylbutane	I6	0.0063	0.0290	0.003	0.003
Cyclopentane	N5	0.0039	0.0147	0.001	0.001
2,3-Dimethylbutane	I6	0.0097	0.0447	0.004	0.004
2-Methylpentane	I6	0.0350	0.1613	0.014	0.014
3-Methylpentane	I6	0.0193	0.0889	0.008	0.008
n-Hexane	P6	0.0327	0.1507	0.013	0.013
2,2-Dimethylpentane	I7	0.0011	0.0059	0.001	0.001
Methylcyclopentane	N6	0.0164	0.0738	0.006	0.006
2,4-Dimethylpentane	I7	0.0022	0.0118	0.001	0.001
2,2,3-Trimethylbutane	I7	0.0007	0.0037	0.000	0.000
Benzene	A6	0.0129	0.0539	0.004	0.004
3,3-Dimethylpentane	I7	0.0007	0.0037	0.000	0.000
Cyclohexane	N6	0.0139	0.0626	0.005	0.005
2-Methylhexane	I7	0.0077	0.0413	0.004	0.004
2,3-Dimethylpentane	I7	0.0020	0.0107	0.001	0.001
1,1-Dimethylcyclopentane	N7	0.0015	0.0079	0.001	0.001
3-Methylhexane	I7	0.0068	0.0364	0.003	0.003
1c,3-Dimethylcyclopentane	N7	0.0020	0.0105	0.001	0.001
1t,3-Dimethylcyclopentane	N7	0.0017	0.0089	0.001	0.001
3-Ethylpentane	I7	0.0004	0.0021	0.000	0.000
1t,2-Dimethylcyclopentane	N7	0.0025	0.0131	0.001	0.001
2,2,4-Trimethylpentane	I8	0.0001	0.0006	0.000	0.000

n-Heptane	P7	0.0100	0.0536	0.005	0.005
1c,2-Dimethylcyclopentane	N7	0.0003	0.0016	0.000	0.000
Methylcyclohexane	N7	0.0181	0.0950	0.007	0.007
2,2-Dimethylhexane	I8	0.0004	0.0025	0.000	0.000
1,1,3-Trimethylcyclopentane	N7	0.0001	0.0006	0.000	0.000
Ethylcyclopentane	N7	0.0005	0.0026	0.000	0.000
2,5-Dimethylhexane	I8	0.0005	0.0031	0.000	0.000
2,2,3-Trimethylpentane	I8	0.0004	0.0025	0.000	0.000
2,4-Dimethylhexane	I8	0.0001	0.0006	0.000	0.000
1c,2t,4-Trimethylcyclopentane	N8	0.0002	0.0012	0.000	0.000
3,3-Dimethylhexane	I8	0.0002	0.0012	0.000	0.000
Toluene	A7	0.0093	0.0458	0.003	0.003
2,3-Dimethylhexane	I8	0.0002	0.0012	0.000	0.000
2-Methylheptane	I8	0.0012	0.0073	0.001	0.001
4-Methylheptane	I8	0.0004	0.0025	0.000	0.000
3-Methylheptane	I8	0.0009	0.0055	0.000	0.000
1c,2t,3-Trimethylcyclopentane	N8	0.0012	0.0072	0.001	0.001
3-Ethylhexane	I8	0.0001	0.0006	0.000	0.000
1t,4-Dimethylcyclohexane	N8	0.0006	0.0036	0.000	0.000
1,1-Dimethylcyclohexane	N8	0.0003	0.0018	0.000	0.000
2,2,5-Trimethylhexane	I9	0.0001	0.0007	0.000	0.000
3c-Ethylmethylcyclopentane	N8	0.0001	0.0006	0.000	0.000
3t-Ethylmethylcyclopentane	N8	0.0001	0.0006	0.000	0.000
2t-Ethylmethylcyclopentane	N8	0.0001	0.0006	0.000	0.000
1t,2-Dimethylcyclohexane	N8	0.0003	0.0018	0.000	0.000
UnknownC7s	U7	0.0001	0.0005	0.000	0.000
n-Octane	P8	0.0014	0.0086	0.001	0.001
1c,4-Dimethylcyclohexane	N8	0.0002	0.0012	0.000	0.000
1,1,4-Trimethylcyclohexane	N9	0.0001	0.0007	0.000	0.000
Ethylcyclohexane	N8	0.0001	0.0006	0.000	0.000
n-Propylcyclopentane	N8	0.0001	0.0006	0.000	0.000
1c,3c,5-Trimethylcyclohexane	N9	0.0001	0.0007	0.000	0.000
2,5-Dimethylheptane	I9	0.0001	0.0007	0.000	0.000
Ethylbenzene	I8	0.0001	0.0006	0.000	0.000
1,3-Dimethylbenzene (m-Xylene)	A8	0.0005	0.0028	0.000	0.000
1,4-Dimethylbenzene (p-Xylene)	A8	0.0002	0.0011	0.000	0.000
1,2-Dimethylbenzene (o-Xylene)	A8	0.0001	0.0006	0.000	0.000
TOTAL		100.00000	100.00000	2.0817	2.0926

CALCULATED VALUES**

BTEX COMPONENTS	MOLE%	WT%	BTU @	14.65	14.73
BENZENE	0.0129	0.0539	LHV NET DRY REAL :	945.9 /scf	951.0 /scf
TOLUENE	0.0093	0.0458	NET WET REAL :	929.4 /scf	934.5 /scf
ETHYLBENZENE	0.0001	0.0006	HHV GROSS DRY REAL :	1047.5 /scf	1053.2 /scf
XYLENES	0.0008	0.0045	GROSS WET REAL :	1029.2 /scf	1034.9 /scf
TOTAL BTEX	0.0231	0.1048	NET HEATING VALUE (60 °F ideal reaction):		19218.9 Btu/lbm
			GROSS HEATING VALUE (60°F ideal reaction):		21283.2 Btu/lbm
			RELATIVE DENSITY (AIR=1):		0.6453
			DENSITY		0.04927 lb/scf
			COMPRESSIBILITY FACTOR :		0.9975
			REGULAR WOBBE INDEX		1304.9

*(DETAILED HYDROCARBON ANALYSIS/NJ 1993)
Mod ASTM D6730, GPA 2261 & GPA 2286.

** (CALC. GPA 2172, GPA 2145 & TP-17 @14.696 & 60 F)

C6+ Fraction of DHA Gas Analysis @60°F, 14.696 psia

Net Dry Ideal BTU	<u>4538.5</u> /scf	Relative Density - SG (Air=1)	<u>3.1205</u>	C6+ factors
Gross Dry Ideal BTU	<u>4878.5</u> /scf	Z Compressibility Factor	<u>0.99075</u>	<u>0.99012</u>
Net Dry Ideal BTU	<u>19185.6</u> /lb	Density Factor	<u>238.168</u> lbm/1000 ft ³	
Gross Dry Ideal BTU	<u>20622.7</u> /lb	Molar Mass or MW	<u>90.381</u> g/mol	
		Volume Liquid Ideal gas	<u>0.089</u> scf/gal	<u>25.1</u>
This hexanes plus fraction may be applied in place of published C6+ factors. The Z & GPM need additional calc for C6+ factors.				
/DIV/0 or 0 (zero) will appear in this section when there is no hexanes plus in the sample to calculate C6+ factors.				

The data presented herein has been acquired by means of current analytical techniques and represents the judicious conclusion EMPACT Analytical Systems, Inc. Results of the analysis can be affected by the sampling conditions, therefore, are only warranted through proper lab protocol. EMPACT assumes no responsibility for interpretation or any consequences from application of the reported information and is the sole liability of the user. The reproduction in any media of this reported information may not be made, in portion or as a whole, without the written permission of EMPACT Analytical Systems, Inc.