



**EXTENDED NATURAL GAS ANALYSIS (*DHA)
GLYCALC INFORMATION**

PROJECT NO. :	202405125	ANALYSIS NO. :	01
COMPANY NAME :	CAERUS OIL & GAS LLC	ANALYSIS DATE:	MAY 30, 2024 12:40
ACCOUNT NO. :		SAMPLE DATE :	MAY 23, 2024 7:30
PRODUCER :	CAERUS PICEANCE LLC	CYLINDER NO. :	ECA-822
LEASE NO. :	110170021	SAMPLED BY :	ALEX GALLEGOS
NAME/DESCRIP :	GG3 CHEVRON 33-7D CASING		

FIELD DATA

SAMPLE PRES. :	339	SAMPLE TEMP. :	43
H2S BY STAIN TUBE:	—	AMBIENT TEMP.:	
COMMENTS :	SPOT ppm mol NO PROBE Possible moisture observed.		

<u>Componet</u>	<u>Mole %</u>	<u>Wt %</u>
Helium	0.00	0.00
Hydrogen	0.06	0.01
Carbon Dioxide	2.15	5.02
Nitrogen	0.08	0.12
Methane	87.2770	74.2959
Ethane	7.1851	11.4642
Propane	1.9815	4.6364
Isobutane	0.4687	1.4455
n-Butane	0.3430	1.0579
Isopentane	0.1691	0.6473
n-Pentane	0.0858	0.3285
Cyclopentane	0.0032	0.0119
n-Hexane	0.0299	0.1367
Cyclohexane	0.0087	0.0388
Other Hexanes	0.0772	0.3516
Heptanes	0.0337	0.1783
Methylcyclohexane	0.0109	0.0568
2,2,4 Trimethylpentane	0.0000	0.0000
Benzene	0.0028	0.0116
Toluene	0.0014	0.0068
Ethylbenzene	0.0001	0.0006
Xylenes	0.0004	0.0023
C8+ Heavies	0.0252	0.1679
<u>Subtotal</u>	<u>99.99370</u>	<u>99.98900</u>
Oxygen/Argon	0.00	0.00
Alcohols	0.0063	0.0110
<u>Total</u>	<u>100.00000</u>	<u>100.00000</u>

	<u>Total</u>	<u>C6+</u>	<u>C8+</u>	<u>C10+</u>
Calculated Values BTU @ 14.65	Sample	Fraction	Fraction	Fraction
LHV Net Dry Real:	998.3	4723.1	5764.9	6610.4 Btu/scf
Net Wet Real:	980.8	4640.5	5664.1	6494.8 Btu/scf
HHV Gross Dry Real:	1104.5	5082.9	6160.3	7029.7 Btu/scf
Gross Wet Real:	1085.2	4994.0	6052.6	6906.8 Btu/scf
Other Calculated Values				
Regualr Wobbe Index*	1370.0	2801.5	2966.3	3239.6 Btu/scf
Net Heating Value (60 °F ideal reaction):	20116.6	18906.9	17080.5	18316.1 Btu/lbm
Gross Heating Value (60°F ideal reaction):	22255.4	20344.7	18249.9	19478.5 Btu/lbm
Molar Mass (MW):	18.84485	94.29	125.493	137.092 g/mol
Relative Density (AIR=1):	0.6506	3.2554	4.3325	4.7333 SG
Density:	0.04966	0.24848	0.33070	0.36125 lbm/scf
Compressibility Factor:	0.9973	0.9913	0.9991	0.9995 Z
Liquid Volume real gas @:	14.65	17.9766	0.0768	0.01 gal/1000 scf

* The Wobbe pressure base in the number considered is based upon the given Pb of the HHV above.
 #DIV/0 or 0 (zero) will appear in the Calculated Value Section when there is no C6+, C8+ or C10+ in the sample to calculate these factors.
 BDL - Below Detection Limit. The H2S LOS has a detection limit of 0.25 ppm. A _ (an underscore) indicates there was no tube pulled for H2S.

The data presented herein has been acquired by means of current analytical techniques and represents the judicious conclusion EMPACT Analytical Systems, Inc. Results of the analysis can be affected by the sampling conditions, therefore, are only warranted through proper lab protocol. EMPACT assumes no responsibility for interpretation or any consequences from application of the reported information and is the sole liability of the user. The reproduction in any media of this reported information may not be made, in portion or as a whole, without the written permission of EMPACT Analytical Systems, Inc.



EXTENDED NATURAL GAS ANALYSIS (*DHA)

DHA COMPONENT LIST

PRIMARY DB KEY: **05-045-09022** NAME/DESCRIP : **GG3 CHEVRON 33-7D**
 LEASE #: **110170021** CASING
 FIELD/AREA: **GRAND VALLEY - #31290**

 PROJECT NO. : **202405125** ANALYSIS NO. : **01**
 COMPANY NAME : **CAERUS OIL & GAS LLC** ANALYSIS DATE: **MAY 30, 2024 12:40**
 OFFICE / BRANCH: **PARACHUTE, CO** SAMPLE DATE : **MAY 23, 2024 7:30**
 CUSTOMER REF: TO:
 PRODUCER : **CAERUS PICEANCE LLC** EFFECTIVE DATE:
*****FIELD DATA*****
 SAMPLE CYCLE: SAMPLE TYPE: **SPOT**
 SAMPLE PRES. : **339** psig PROBE : **NO**
 FLOW PRES. : psig CYLINDER NO. : **ECA-822**
 LAB PRES: psig SAMPLED BY : **ALEX GALLEGOS**
 SAMPLE TEMP. : **43** °f SAMPLING COMPANY: **CAERUS OIL & GAS LLC**
 AMBIENT TEMP.: °f H2S BY STAIN TUBE: **-** ppm mol
 H2O BY STAIN TUBE: **-** #/mmcf CO2 BY STAIN TUBE: **-** Mol %
 FIELD COMMENTS:
 LAB COMMENTS: **Possible moisture observed.**

COMPONENT	PIANO #	MOLE %	MASS %	GPM @ 14.65	GPM @ 14.73
Helium	---	0.00	0.00	---	---
Hydrogen	---	0.06	0.01	---	---
Oxygen/Argon	---	0.00	0.00	---	---
Nitrogen	---	0.08	0.12	---	---
Carbon Dioxide	---	2.15	5.02	---	---
Methane	P1	87.2770	74.2959	---	---
Ethane	P2	7.1851	11.4642	1.916	1.927
Propane	P3	1.9815	4.6364	0.545	0.548
i-Butane	I4	0.4687	1.4455	0.153	0.154
Methanol	X1	0.0062	0.0106	0.001	0.001
n-Butane	P4	0.3430	1.0579	0.108	0.109
2,2-Dimethylpropane	I5	0.0046	0.0176	0.002	0.002
i-Pentane	I5	0.1645	0.6297	0.060	0.060
n-Pentane	P5	0.0858	0.3285	0.031	0.031
2,2-Dimethylbutane	I6	0.0056	0.0256	0.002	0.002
Cyclopentane	N5	0.0032	0.0119	0.001	0.001
2,3-Dimethylbutane	I6	0.0088	0.0402	0.004	0.004
2-Methylpentane	I6	0.0331	0.1513	0.014	0.014
3-Methylpentane	I6	0.0175	0.0800	0.007	0.007
n-Hexane	P6	0.0299	0.1367	0.012	0.012
2-Butanol	X4	0.0001	0.0004	0.000	0.000
2,2-Dimethylpentane	I7	0.0011	0.0058	0.001	0.001
Methylcyclopentane	N6	0.0122	0.0545	0.004	0.004
2,4-Dimethylpentane	I7	0.0020	0.0106	0.001	0.001
2,2,3-Trimethylbutane	I7	0.0005	0.0026	0.000	0.000
Benzene	A6	0.0028	0.0116	0.001	0.001
3,3-Dimethylpentane	I7	0.0006	0.0032	0.000	0.000

Cyclohexane	N6	0.0087	0.0388	0.003	0.003
2-Methylhexane	I7	0.0071	0.0377	0.003	0.003
2,3-Dimethylpentane	I7	0.0015	0.0080	0.001	0.001
1,1-Dimethylcyclopentane	N7	0.0011	0.0057	0.000	0.000
3-Methylhexane	I7	0.0058	0.0308	0.003	0.003
1c,3-Dimethylcyclopentane	N7	0.0015	0.0078	0.001	0.001
1t,3-Dimethylcyclopentane	N7	0.0013	0.0068	0.001	0.001
3-Ethylpentane	I7	0.0002	0.0011	0.000	0.000
1t,2-Dimethylcyclopentane	N7	0.0021	0.0109	0.001	0.001
n-Heptane	P7	0.0084	0.0447	0.004	0.004
1c,2-Dimethylcyclopentane	N7	0.0002	0.0011	0.000	0.000
Methylcyclohexane	N7	0.0109	0.0568	0.004	0.004
2,2-Dimethylhexane	I8	0.0003	0.0018	0.000	0.000
Ethylcyclopentane	N7	0.0003	0.0015	0.000	0.000
2,5-Dimethylhexane	I8	0.0003	0.0018	0.000	0.000
2,2,3-Trimethylpentane	I8	0.0003	0.0018	0.000	0.000
1c,2t,4-Trimethylcyclopentane	N8	0.0002	0.0012	0.000	0.000
3,3-Dimethylhexane	I8	0.0001	0.0006	0.000	0.000
Toluene	A7	0.0014	0.0068	0.000	0.000
2,3-Dimethylhexane	I8	0.0001	0.0006	0.000	0.000
2-Methylheptane	I8	0.0004	0.0024	0.000	0.000
4-Methylheptane	I8	0.0001	0.0006	0.000	0.000
3-Methylheptane	I8	0.0002	0.0012	0.000	0.000
1c,2t,3-Trimethylcyclopentane	N8	0.0002	0.0012	0.000	0.000
1t,4-Dimethylcyclohexane	N8	0.0001	0.0006	0.000	0.000
1,1-Dimethylcyclohexane	N8	0.0001	0.0006	0.000	0.000
n-Octane	P8	0.0001	0.0006	0.000	0.000
1,1,4-Trimethylcyclohexane	N9	0.0001	0.0007	0.000	0.000
Ethylbenzene	I8	0.0001	0.0006	0.000	0.000
1,3-Dimethylbenzene (m-Xylene)	A8	0.0001	0.0006	0.000	0.000
1,2-Dimethylbenzene (o-Xylene)	A8	0.0003	0.0017	0.000	0.000
i-Propylbenzene	A9	0.0002	0.0013	0.000	0.000
3,6-Dimethyloctane	I10	0.0015	0.0113	0.001	0.001
1,3-Methylethylbenzene	A9	0.0053	0.0338	0.003	0.003
1,4-Methylethylbenzene	A9	0.0025	0.0159	0.001	0.001
1,3,5-Trimethylbenzene	A9	0.0025	0.0159	0.001	0.001
1,2-Methylethylbenzene	A9	0.0020	0.0127	0.001	0.001
2-Methylnonane	I10	0.0001	0.0007	0.000	0.000
3-Methylnonane	I10	0.0001	0.0007	0.000	0.000
t-Butylbenzene	A10	0.0063	0.0449	0.003	0.003
i-Butylbenzene	A10	0.0001	0.0007	0.000	0.000
sec-Butylbenzene	A10	0.0001	0.0007	0.000	0.000
n-Decane	P10	0.0001	0.0007	0.000	0.000
1,2,3-Trimethylbenzene	A9	0.0007	0.0045	0.000	0.000
1,3-Methyl-i-propylbenzene	A10	0.0001	0.0007	0.000	0.000
1,3-Diethylbenzene	A10	0.0001	0.0007	0.000	0.000
1,3-Methyl-n-propylbenzene	A10	0.0001	0.0007	0.000	0.000
1,4-Diethylbenzene	A10	0.0001	0.0007	0.000	0.000
n-Butylbenzene	A10	0.0001	0.0007	0.000	0.000
1,4-Methyl-t-butylbenzene	A11	0.0001	0.0008	0.000	0.000
n-Undecane	P11	0.0001	0.0008	0.000	0.000
UnknownC11s	U11	0.0003	0.0025	0.000	0.000
UnknownC12s	U12	0.0001	0.0008	0.000	0.000
TOTAL		100.00000	100.00000	2.8936	2.9093

BTEX COMPONENTS	MOLE%	WT%	CALCULATED VALUES**		
			BTU @	14.65	14.73
BENZENE	0.0028	0.0116	LHV NET DRY REAL :	998.3 /scf	1003.8 /scf
TOLUENE	0.0014	0.0068	NET WET REAL :	980.8 /scf	986.3 /scf
ETHYLBENZENE	0.0001	0.0006	HHV GROSS DRY REAL :	1104.5 /scf	1110.5 /scf
XYLENES	0.0004	0.0023	GROSS WET REAL :	1085.2 /scf	1091.2 /scf
TOTAL BTEX	0.0047	0.0213	NET HEATING VALUE (60 °F ideal reaction):		20116.6 Btu/lbm
			GROSS HEATING VALUE (60°F ideal reaction):		22255.4 Btu/lbm
			RELATIVE DENSITY (AIR=1):		0.6506
			DENSITY		0.04966 lb/scf
			COMPRESSIBILITY FACTOR :		0.9973
			REGULAR WOBBE INDEX		1370.0

*(DETAILED HYDROCARBON ANALYSIS/NJ 1993)

Mod ASTM D6730, GPA 2261 & GPA 2286.

** (CALC: GPA 2172, GPA 2145 & TP-17 @14.696 & 60 F)

C6+ Fraction of DHA Gas Analysis @60°F, 14.696 psia

Net Dry Ideal BTU	<u>4696.8</u> /scf	Relative Density - SG (Air=1)	<u>3.2554</u>	C6+ factors
Gross Dry Ideal BTU	<u>5054.6</u> /scf	Z Compressibility Factor	<u>0.99131</u>	<u>0.99014</u>
Net Dry Ideal BTU	<u>18906.9</u> /lb	Density Factor	<u>248.477</u> lbm/1000 ft3	
Gross Dry Ideal BTU	<u>20344.7</u> /lb	Molar Mass or MW	<u>94.29</u> g/mol	
		Volume Liquid Ideal gas	<u>0.077</u> scf/gal	<u>23.2</u>

**This hexanes plus fraction may be applied in place of published C6+ factors. The Z & GPM need additional calc for C6+ factors.
#DIV/0 or 0 (zero) will appear in this section when there is no hexanes plus in the sample to calculate C6+ factors.**

The data presented herein has been acquired by means of current analytical techniques and represents the judicious conclusion EMPACT Analytical Systems, Inc. Results of the analysis can be affected by the sampling conditions, therefore, are only warranted through proper lab protocol. EMPACT assumes no responsibility for interpretation or any consequences from application of the reported information and is the sole liability of the user. The reproduction in any media of this reported information may not be made, in portion or as a whole, without the written permission of EMPACT Analytical Systems, Inc.